

NATIONAL TRANSPORTATION SAFETY BOARD **Investigative Hearing**

Norfolk Southern Railway general merchandise freight train 32N derailment with subsequent hazardous material release and fires, in East Palestine, Ohio, on February 3, 2023



Agency / Organization

## **Norfolk Southern Railway**

**Title** 

## **CHARM model BLEVE catastrophic failure theoretical outcomes for East Palestine, Ohio.**

# VC Railcar Catastrophic Failure

Theoretical Outcomes

-- Not Actual -- Developed for Planning Purposes only --

# Disclaimer

- Model was produced in the absence of specific site conditions or details regarding the nature of flame impingement or status of railcar's contents.
- This model could under-predict catastrophic outcomes resulting from conditions not reflected herein.
- The CHARM model was used within the realm of its capacities. Some variables may not be accounted for, thus the model's run details and function calculations have been included for transparency.
- Models can only provide a range of potential outcomes rendered less effective if input data is incorrect or mis-representative.

# Scenario Characteristics

- CHARM Model used (https://www.charmmodel.com/)
- 105J300 VC Railcar
	- 27,600 gallons instantly released by pressure rupture of railcar
	- 48ft tank length, 9.9 ft tank diameter (Greenbrier Pressure Tank Car Specs)
- Explosion overpressure
	- Railcar pressure 225 psi (safety valve rating of 105J300)
	- 27,600 gallons released
	- Detonation (flame speed Mach 1) occurring < 1s after vapor release
- BLEVE Radiation
	- Depicts thermal radiation as a result of fireball from full vapor detonation

# Explosion Overpressure

Depicting pressure wave from vapor cloud explosion 1 second after total railcar release.

#### $7.0$ **EXPLOSION OVERPRESSURES**

CHARM calculates overpressures or shockwave pressures for two scenarios: a sphere bursting due to failure of the vessel and an unconfined vapor cloud explosion. Both of these phenomena are modeled using methods from Baker et al. (1983).

#### $7.1$ **Sphere Burst Overpressure**

Although the equations described here are strictly for the mechanical failure of a pressurized sphere, they are used for all cases of pressurized failure. A mechanical failure, such as in an instantaneous gas release, is always assumed to be from a spherical vessel.

Two important factors in a pressurized vessel failure shockwave calculation are the storage pressure and the amount of material stored. Pressure has the units of energy density and describes the amount of energy available for shockwave formation.

The equation for calculating the maximum overpressure of a sphere burst is provided by Liepman and Roshko (1967):

$$
\frac{p_1}{p_0} = \frac{p_{s0}}{p_0} \left\{ 1 - \frac{\left(\gamma_1 - 1\right) \left(\frac{a_0}{a_1}\right) \left(\frac{p_{s0}}{p_0} - 1\right)}{\sqrt{2 \gamma_0 \left[2 \gamma_0 + \left(\gamma_0 + 1\right) \left(\frac{p_{s0}}{p_0} - 1\right)\right]}} \right\}^{\left(\frac{-2\gamma_1}{\gamma_1 - 1}\right)}
$$

 $(7-1)$ 

where  $p_1$  $=$  pressure inside the sphere;

> = atmospheric pressure;  $p_0$

 $=$  air shock pressure at the instant of burst;  $p_{s0}$ 

$$
V_1 = C_p/C_v
$$
 for gas in sphere;

$$
\gamma_0 = C_p/C_v \text{ for air};
$$

 $C_p$ = specific heat at constant pressure;

- = specific heat at constant volume;  $C_v$
- $=$  speed of sound in air; and  $a<sub>0</sub>$
- $=$  speed of sound in sphere;  $a<sub>1</sub>$

The parameter that must be solved for by iteration, is  $p_{s0}/p_0$ .

The value used in CHARM is the overpressure  $(\overline{P}_s)$ , which is defined as follows:

### Complex Hazardous Air Release Model (CHARM®)

### **Technical Reference Manual**

### By Mark W. Eltgroth, Ph.D.

 $\overline{P}_s = \frac{p_s}{p_0} - 1$  $(7-2)$ 

At the sphere surface, the overpressure equation is:

$$
\overline{P}_{s0} = \frac{P_{s0}}{P_0} - 1 \tag{7-3}
$$

The other parameter required for predicting the overpressure at distances downwind is an energy-scaled radius ( $\overline{R}$ ). At the surface of the sphere, the energy-scaled radius ( $\overline{R}$ <sub>1</sub>) given by Baker is:

$$
\overline{\mathbf{R}}_1 = \left[\frac{3(\gamma_1 - 1)}{4\pi \left(\frac{\mathbf{p}_1}{\mathbf{p}_0} - 1\right)}\right]^{\frac{1}{3}} = \frac{\mathbf{r}_1}{\mathbf{R}_0}
$$
\n7-4

where 
$$
r_1
$$
 = radius of the sphere;  
\n $R_0$  = energy radius  
\n
$$
= \left(\frac{E}{p_0}\right)^{\frac{1}{3}}
$$
\n
$$
E = \left(\frac{p_1 - p_0}{\gamma_1 - 1}\right) V_1; \text{ and}
$$
\n
$$
V_1
$$
 = volume of sphere.

Once the values of  $\overline{P}_s$  and  $\overline{R}$  are known at the sphere surface, a curve that agrees with these values can be selected from Figure 7-1. Once a curve is selected, if either value,  $\overline{R}$ or  $\overline{P}_s$ , is known, the other can be calculated. The curves shown in Figure 7-1 have been digitized, and CHARM interpolates the actual curve to use once the conditions at the sphere surface are known. The dimensional pressure and radius can be found by multiplying the dimensionless overpressures and radii by  $p_0$  and  $R_0$ , respectively.





#### **Overpressure Damage Estimates**

The following are the peak pressures formed in excess of normal atmospheric pressure by blast and shock waves:

#### Overpressure (psi)



Source: Lees, F.P, Loss Prevention in the Process Industries, Vo,. 1, Butterworths, London and Boston, 1980.



# Study - projectile range of fragments from VC BLEVE Events – analysis of > 100 vessel failures

"The range distribution for LPG, vinyl chloride monomer and ammonia are fairly similar, although no very long ranges have been observed in this sample from ammonia vessels. As a rough guideline it might be assumed that 80% of fragments will travel less than 200m, the remainder travelling anything up to about 1km."

Holden, P. L., & Reeves, A. B. (1985). Fragment hazards from failures of pressurized liquefied gas vessels. In *IchemE symposium series* (Vol. 93, pp. 205-220).

IChemE SYMPOSIUM SERIES No. 93



FIG. 3 RANGE Vs. % FRAGMENTS FOR VARIOUS CHEMICALS

# BLEVE Radiation

Depicting thermal radiation resulting from BLEVE and subsequent fireball of vapor

#### **FIREBALL/BLEVE ALGORITHM**  $5.0$

The Fireball/BLEVE (Boiling Liquid Expanding Vapor Explosion) algorithm is one of the simplest in CHARM; only a few equations must be solved. The method comes from Moorhouse and Pritchard (1982) and Roberts (1982). Instead of being derived from fundamental principles, the BLEVE equations are parametric.

#### $5.1$ **Calculation of the Efficiency of Explosion**

An efficiency of explosion is either entered by the user or calculated by CHARM. If calculated, the explosion efficiency  $(v)$  is a function of the vapor pressure of the material and is:

$$
v = 0.27 P_{\rm s}^{0.32} \tag{5-1}
$$

where  $P_S$  $=$  vapor pressure in Pascals of the chemical at the storage pressure.

The radius  $(R_f)$  of the ensuing fireball (in meters) is calculated as follows:

$$
R_f = 2.665 \, m_{kg}^{0.327} \tag{5-2}
$$

where 
$$
m_{kg}
$$
 = mass of material in kilograms involved in the explosion

The duration (Tf) of the fireball in seconds is given as:

$$
T_{\rm f} = 1.089 \, \rm m_{kg}^{0.327} \tag{5-3}
$$

Finally, the amount of radiation (W) being emitted is given as:

$$
W = \frac{H_c m_{kg} v 1000}{T_f}
$$
 (5-4)

where W  $=$  energy emission rate in watts; and

Hc = heat of combustion of the material in Joules per gram.

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#### **Calculation of Fluxes**  $5.2$

Once the energy emission rate (W) is calculated, the fluxes can be determined at any distance from the source. The fireball is assumed to be a point source. As such, the flux (F) at some distance (r) from the fireball can be calculated using the inverse square property of radiation:

$$
F = \frac{W}{4\pi r^2}
$$
 (5-5)

Because the fireball is assumed to be a point source, either F or r can be specified and the other parameter calculated.

#### **BLEVE** Radiation 4

### 105J300 Vinyl Chloride Railcar<br>Species: Vinyl Chloride





Duration: 46.7 sec Heat Rate: 6.42e+06 kW Flame center:  $0$  ft Flame radius: 075 ft<br>Flame radius: 075 ft<br>Burn Efficency: 0.16<br>RMP Dist: 1049 ft



#### **Thermal Radiation Damage Estimates**

The following are thermal radiation flux values and the expected damage estimates associated with each:



Source: Guidelines for Chemical Process Quantitative Risk Analysis, American Institute of Chemical Engineers Center for Chemical Process Safety, NY, NY, 1989.

